

MODELING OF DARK FERMENTATION PROCESS FOR VOLATILE FATTY ACIDS PRODUCTION

By

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Abstract

Modeling of Volatile fatty acids under anaerobic condition dark fermentation process

Master of Engineering, 2018

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Civil Engineering

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This study examined the fermentation process for the production of volatile fatty acids from the organic waste. The depletion of fossil fuels motivated researchers to search for alternative energy and fuels instead of relying on the non-renewable way of energy and fuel production. Anaerobic digestion is a biochemical process in the absence of oxygen, where complex organic matter are degraded. The different stages of anaerobic digestion and important operating parameters such as pH, temperature and retention time. The most suitable feedstock and its effects on the treatment process are discussed.

This study evaluates the modelling of VFAs production. The paper also demonstrates various model like ADM1, surface limiting model, and steady-state model. Furthermore, an experimental setup consisting of two semi-continuous reactors was employed for the sample analysis. The reactors were fed with raw and pre-treated source separated organics with solid retention time of 3 days.

Keywords: Anaerobic digestion, Feedstocks, SSO, VFAs, ADM1.

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1 Introduction

In the modern era, one of the biotechnologies developed is to utilize the waste for useful energy and material recovery using anaerobic digestion. Municipal waste contributes to environmental problems including habitat destruction, surface and groundwater pollution and increased emission of greenhouse gases and the impact on climate change. In 2008, Canadian household generated 777 kg per capita annually municipal waste which was twice as much as Japan. In the same year, 8.5 million tons of waste out of 13 million were disposed of in landfills. Landfills are the most common in Canada, but there is environmental concern about landfills like leachate and gases that contaminate groundwater and surface water (R. Hester, 2002). To achieve more sustainable municipal waste, the treatment of this waste is an essential concern for solid waste management and to reduce the toxicity and volume of waste disposal in landfills. The anaerobic digestion technology is one of the leading options for processing the organic material in municipal solid waste (Verma, 2002).

The most prominent method for production of methane gas from organic matter is high rate anaerobic digesters. Anaerobic digestion has become the main biological process to treat the organic matter. In the end stage of the process, the end products are methane gas, carbon dioxide and highly nutritive digestate which can be further used as fertilizers for the soil. Anaerobic digestion is a most efficient process to treat and utilize food waste for energy recycling (Muzaffar Ahmad Mir, February 2016). Also, anaerobic digestion is used to obtain volatile fatty acids in metabolic intermediates in the acidification step of the AD process. (Tânia Gameiro, September 2016)

Fermentation technology is receiving revived recognition as a sustainable and economically technology to produce a variety of energy through the process such as methane, ethanol, butanol, and hydrogen from a waste material through anaerobic digestion which is inexpensive and renewable (Silva, 2014). Anaerobic fermentation is an effective bioprocess for the production of volatile fatty acids and another organic compound such as alcohol. Also, anaerobic fermentation of organic waste with high hydrolysis rate can process for biogas production. The VFA production and other

composed mixture by hydrolytic – acidogenic fermentation of organic waste have a significant influence on the performance of the process and other applications.

2 Anaerobic Digestion

2.1 Background

Anaerobic biological treatment is well understood and used frequently as anaerobic digesters to treat complex organic solid waste. Anaerobic digestion treatment has been one of the effective treatment options for biodegradable organic waste including food waste, animal manure, and sewage sludge as it effectively reduces the amount of organic waste and produces biogas as renewable energy (Dong-Jin Lee, 2015). In the past, aerobic treatment was preferred, i.e. in the presence of oxygen in the treatment of wastewater as it was easy to operate. In comparison, anaerobic reactors were assumed to be less stable and more expensive to install, but this belief was due to the limited knowledge of the process and reactor design.

The application of anaerobic treatment has gradually increased in the past three decades. Due to the significant advantages of aerobic treatment, anaerobic treatment has emerged as a practical and economical process for the solid waste.

2.2 What Is Anaerobic Digestion?

Anaerobic digestion is the biological process that breaks down organic material in the absence of oxygen into methane and carbon dioxide. Organic materials are composed of organic compounds resulting from decomposition of previously living organisms such as plants and animal and their waste products. In figure 1 configuration of the anaerobic digester is illustrated. There are several different sources of organic material for anaerobic digestion such as municipal wastewater, food waste, and fats, etc. The end product of anaerobic digestion is biogas which is mainly composed of methane nearly about 60-70% by volume and carbon dioxide about 30-40% by volume along with some amount of

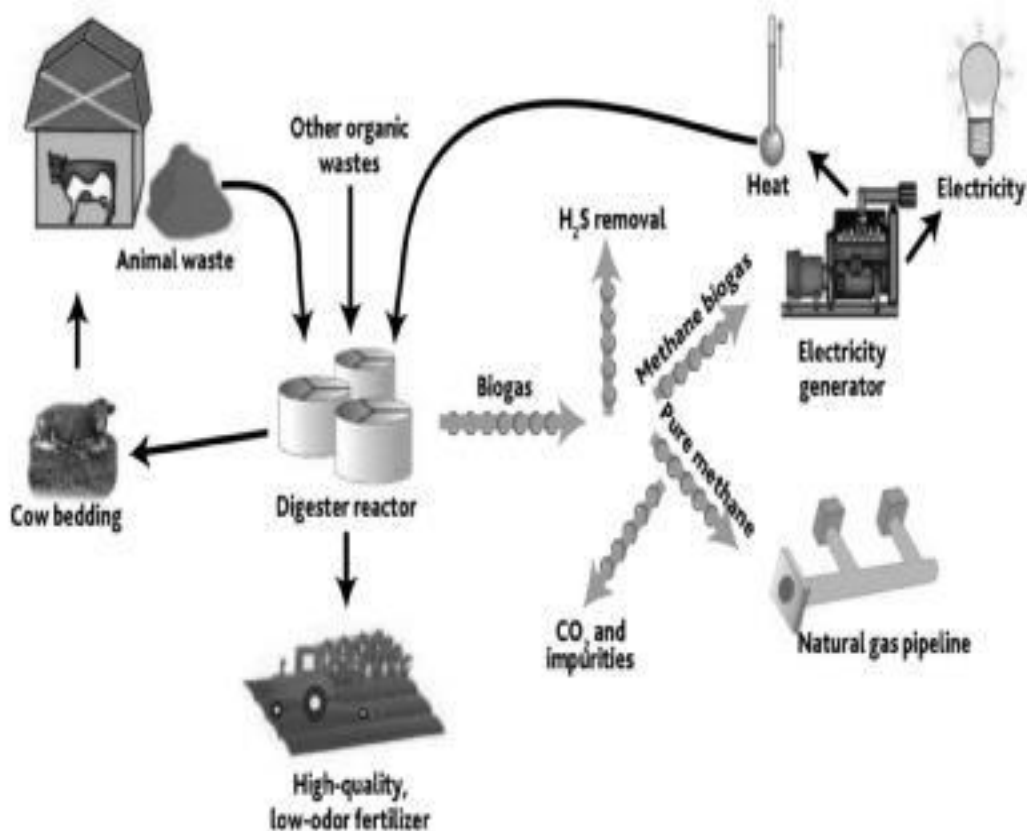


Figure 1: Anaerobic digester configuration source (Neibling, June 2014)

hydrogen sulphide and trace Gases. Biogas can be used for heat production, generate electricity and renewable natural gas. (Chen, June 2014)

Digested solid left over after the treatment can be composted and utilized as agricultural fertilizers as it is rich in nutrients. The AD is carried out at different temperature conditions, such as mesophilic and thermophilic, and various other factors which can alter the process in numerous ways is described briefly later (Muzaffar Ahmad Mir, February 2016).

3 Anaerobic Digestion Process.

Anaerobic biodegradation of organic material proceeds in the absence of oxygen and presence of the anaerobic microorganism. The various factor that depends on the removal efficiency of the organic matter such as nature and composition of organic matter

depends on wastewater characterization, whereas sludge retention time and loading rate depend on the design of treatment system. Figure 2 shows the four steps for anaerobic digestion and their products for each phase. Anaerobic digestion (AD) occurs in four different phases namely:

- I. Hydrolysis
- II. Acidogenesis
- III. Acetogenesis and
- IV. Methanogenesis.

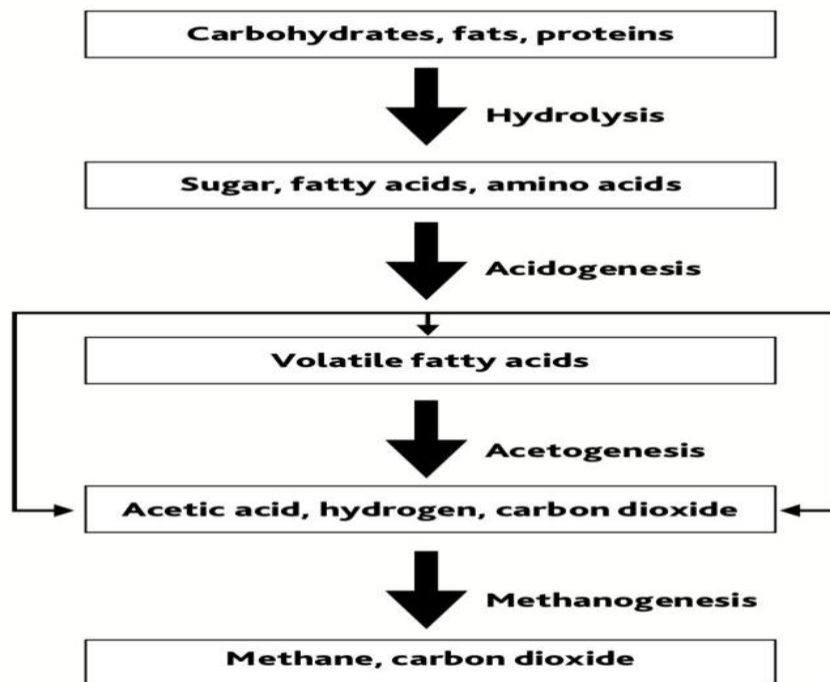


Figure 2: Four steps for anaerobic digestion source (Chen, June 2014)

3.1 Hydrolysis

In the first stage of AD process, fermentative bacteria convert the insoluble complex organic matter into soluble organic matter such as cellulose into sugar, amino acid, and fatty acids, i.e., to compounds suitable for use as a source of energy. This step is carried

out by strict anaerobes such as bactericides, clostridia, and facultative bacteria. The following equation represents the overall reaction:



The first phase is critical due to the large organic molecules which are too large to be directly absorbed and used by microorganism as a food source. To accomplish biodegradation, specific microorganism produces different types of enzymes which break down the large molecules into the smaller pieces that the microorganism can be absorbed and use as a source of energy. Some microorganism emits several different enzymes, which allow them to break down different types of organic materials. A microorganism that breaks down into different sugars is called saccharolytic, while those that break down proteins are called proteolytic. The rate of decomposition during the hydrolysis state depend significantly upon the nature of the substrate (Kayode Feyisetan Adekunle, 2015).

3.2 Acidogenesis

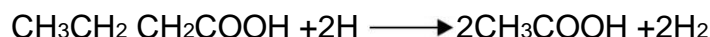
The second stage is Acidogenesis, the reason to call this is because of the fermentative process, the dissolved organic compound in the form of amino acids and sugars will be converting into the volatile fatty acids, alcohols, lactic acid and mineral compounds like hydrogen sulfite, ammonia, carbon dioxide, etc. The pH of the system will be coming down at this stage because a lot of different types of organic acids will be generated in the process for example if the partial pressure of the hydrogen is high, it would decrease the number of reduced compounds. The following equations represent the overall reaction:



In this study, I will emphasize more on the production of volatile fatty acids in dark fermentation process, but it is important to study the whole process taking place to know its end products for various other uses.

3.3 Acetogenesis

In the third stage, the product produced in the second phase is consumed by the substrate for the other microorganism. The product produced after the fermentation process are long chain fatty acids, so these long fatty acids cannot be converted directly to methane, so methanogenic bacteria are converted into the methanogenic substrate, volatile fatty acids, and alcohols. Further volatile fatty acids are oxidized into methanogenic substrates like acetic acid, hydrogen and carbon dioxide. Volatile fatty acids with longer carbon chain are oxidized into acetate and hydrogen. Oxidation reaction will only occur if the partial pressure of hydrogen is low, which explain the collaboration of methanogens is important so that hydrogen is continuously consumed to produce methane (Kayode Feyisetan Adekunle, 2015). Acetogenesis reaction is shown below:



3.4 Methanogenesis

This stage is most critical and slowest biochemical reaction of the process. Methane-producing bacteria are strict anaerobes and are vulnerable to even small amounts of oxygen. Methane production is higher is from the reduction of carbon dioxide with hydrogen.



4 Feedstocks

Several feedstocks exist for the anaerobic digestion process, most of which comprise of organic matter and is suitable for treating anaerobic digestion which includes municipal solid waste, sewage sludge, green waste and organic industrial and commercial wastes. Feedstock characteristics are important factors affecting biogas production during anaerobic digestion. The primary feedstock characteristics comprise of moisture content, total solids, volatile solids, BOD, COD, carbon, and nitrogen. High concentration of VFAs and ammonia (NH_3) can cause toxicity and failure. Figure 3 dramatize several feedstocks for the treatment, and its description is described below.

4.1 Industrial waste and wastewater

Organic industrial and waste include a wide range of waste material from industrial and commercial operating which may form the suitable feedstock for the AD. Waste in high moisture content is suitable for the AD. AD for industrial wastewater is increasing rapidly as it is suitable for wastewater with COD content up to 50,000 mg/L and no oxygen supply are required for the treatment (Monnet, 2003).

4.2 Sewage sludge

Sewage sludge is highly active material produced for the biological treatment plant which starts fermentation on anaerobic condition. Sewage sludge is usually in liquid form with approximately 5% total solids (TS) (Monnet, 2003). Sewage sludge is a well-established technology as it is suitable to improve the dewatering capability and to obtain energy at low operational cost. In the digestion plant, the addition of sludge waste with MSW will increase the nutrient level as well as moisture content.

4.3 Municipal solid waste

The anaerobic digestion of municipal solid waste is entirely feasible. The fundamental issue in this is only that organic waste should be collected separately or has to be

removed mechanically. The high quality product can be achieved if the process is well designed and run (Monnet, 2003). The main disadvantage is the source separation which involves new containers and vehicles for the collection which may result in higher cost. Also, it depends upon the purpose of the plant, if the purpose is to maximize the production of methane then the mixed collection is suitable.

4.4 Green waste

Green waste is garden and parks waste. These wastes need to be shredded to give more homogenous feedstock. It may contain woody lignin which is not biodegradable. Lignin roughly constitutes around 30% wood, and its biodegradability can be increased through some physical and chemical processes, but such processes were only used when plant materials are to be degraded anaerobically else it will increase the treatment cost (Monnet, 2003).



Figure 3: Several feedstocks for treatment source (Steffen & Szolar, 1998)

5 General Process Description

The anaerobic digestion process is used in the treatment of domestic and industrial wastewater. In the process, both solid waste, as well as liquid organic waste, can be anaerobically treated. The aim of this process is not only to produce the methane but also reduce the volume of solid waste. The organic waste that feeds the anaerobic process is composed of carbon, nitrogen, and oxygen. Microorganism uses those organics as a substrate for growth and accommodates with water to form carbon dioxide and methane (Jarvie, 2017). The actual breakdown of organics to its end product methane is not performed by a single process but occurs in different steps which were already described above.

The process of the AD is divided into four stages:

- I. Pre-treatment
- II. Digestion
- III. Gas upgrading &
- IV. Digestate treatment

The pre-treatment depends upon the type of feedstock like manures are mixed whereas MSW is separated and sorted. In the second stage, different kind of digester depending on the solid content, the digester can be dry or wet with different temperature and mixing devices. The temperature plays a crucial role here as the efficiency of the digester depends on the temperature. In the third stage, the impurities present can damage boilers and engine, so the gas was upgraded. For the upgradation, hydrogen sulphide and water vapours are removed from the boilers. The figure 4 below shows the process of digestion when two different types of waste are mixed in digestion plant (Monnet, 2003).

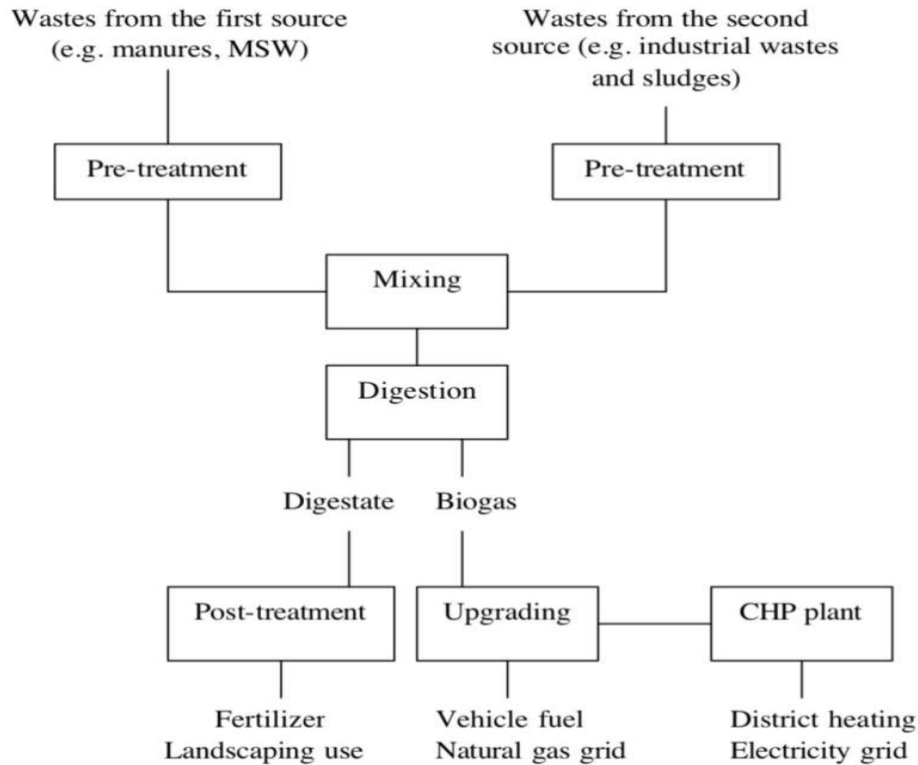


Figure 4: General process for anaerobic digestion plan
Source (Monnet, 2003)

6 Environmental Factors & Operational Parameters Influencing AD

Anaerobic digestion performance can be affected by several factors such as loading, temperature and mixing. More details on the known factors are listed below.

6.1 Total Solid Content

There are different ranges of solid content: low solid contains 10% TS, medium solid range from 15-20% TS and high solid from 22-40% TS. With the increase in the total solid content, the volume of the digester decreases (Jing, 2014).

6.2 Organic Loading Rate

Organic loading rate (OLR) is a measure of biological conversion capacity of the AD system. Feeding the system above its sustainable OLR results in low biogas yield due to the build-up of inhibiting substances such as fatty acids in the digester slurry. Under such circumstances, the feeding rate of the system must be reduced. OLR is a particularly important control parameter in continuous systems. Many plants have reported system failure due to overloading. It is linked with retention time for any particular feedstock and anaerobic reactor volume (Verma, 2002).

6.3 Temperature

Temperature is one of the most important parameters in anaerobic digestion. It determines the rate at which process works for hydrolysis and Methanogenesis (Nayono, 2010). The AD can occur in two stages of temperature 1) mesophilic (25-45⁰C) and 2) thermophilic (45-65⁰C) (CHEN, July 2010). Most of the full-scale AD are operated at mesophilic temperature due to several advantages like high organic removal rate, a high degree of degradation, and solid stabilization. Microbial communities involved in the digestion are sensitive to low temperature so thermophilic digesters are more efficient in terms of retention time, loading rate and gas production but they need higher heat input which makes the process more complicated than mesophilic digestion (Verma, 2002).

6.4 power of Hydrogen (pH)

pH is a significant factor in keeping functional anaerobic digestion. The acid concentration in the aqueous system is expressed by pH value that means the concentration of hydrogen ions. Under neutral conditions, the solution has a value of pH 7. While the acid solution has a pH value less than 7 whereas alkaline solution has been at a higher value of pH 7. In case of an AD, the process requires two different pH values for acidification process and Methanogenesis process. Acetogenesis can lead to accumulation of acids which will drop the pH during fermentation. To maintain the stability of the operation,

bicarbonate and carbonate are added as alkalinity buffer to neutralize volatile fatty acids and carbon dioxide (CHEN, July 2010).

As the digestion reaches the Methanogenesis stage, the pH value can reach above 8 as an increase in the concentration of ammonia. Once methane production is stabilized, the pH level remains between 7.2- 8.2 (Verma, 2002).

6.5 Hydraulic Retention Time

Hydraulic retention time (HRT) is the average time that sludge resides in the digester. If HRT is shorter, the system will fail due to the washout of slowest growing microorganisms that are necessary for the anaerobic process. HRT of solid waste typically varies from 3-55 days depending on the type of waste, temperature, and configuration of digesters. HRT for dry anaerobic digestion lies between 14-30 days whereas for wet anaerobic digestion it can be as low as 3 days (Nayono, 2010).

6.6 Solid Retention Time

In the studies, it was found that volatile fatty acids yields increased with a solid retention time (Zhang, Li, Jia, Dai, & Zhao, Sept 2015). The retention is the time taken by organic matter to complete the degradation process. The optimum value for the SRT will be a function of waste composition, operating temperature and various other process. The SRT is very important to design parameter for carbon conversion as it has to be in the reactor for the optimum time to perform metabolism and produce methane. (Manser, January 2015).

6.7 Mixing

Reactor mixing is a compelling operational parameter for anaerobic digesters. Three types of mixing used in anaerobic digestion system are continuous, intermittent and minimal. Regarding the mixing types, there are conflicts between the result for each type (Manser, January 2015). So far, continuous mixing improved production of methane as compared to another mixing. To eliminate the energy demand for mixing additional research can be carried out for better knowledge and understanding.

6.8 Other Parameters

Chemical additives can enhance the VFA production during anaerobic digestion. Additives like sodium dodecyl benzene sulfonate (SDBS) and β -cyclodextrin can change the surface properties and improve the dissolubility of excess sludge. Increase in VFA production will lead to decrease in methane production. It was also noted that VFA production increased significantly regardless of any mesophilic or thermophilic temperature conditions. These additives are costly, but there might be some cheap and environmentally friendly additives which can help to improve the VFA production during anaerobic digestion of excess sludge (Khan, 2016).



Figure 5 : Operational parameters for anaerobic digestion Source (Yang, 15 December 2015)

7 Literature Review for Volatile Fatty Acid Models

7.1 Introduction

Volatile fatty acids (VFA) are the intermediate product formed in acidification of AD process in which most ordinary are short-chain fatty acids with two to six carbons like acetic, butyric, and propionic acid. These intermediate products in the AD process may be biologically produced from organic waste such as carbon sources, such as waste activated sludge, food waste, paper mill effluent and soft drink wastewater.

Fermentation of organic waste to produce VFA help in reduction of carbon footprint and waste disposal. For VFA production, the process occurs in two steps first hydrolysis of organic matter to soluble compounds and second step acidification of the soluble compounds from hydrolysis to products such as VFA, lactate, and ethanol. The hydrolysis and acidification are a function of various operational parameters which are already discussed in section 3.1. Appels et al., 2008 stated that mainly acetic and butyric acids are produced at low pH using wasted activated sludge whereas pH near 8 mainly produced propionic acid. Lee et al., in his report also stated, higher propionic acid was produced at pH 4 from dairy wastewater (Lee, 2014). Regarding VFA production, total solids (TS) content inside the reactor also depends on the efficiency of the process taking place. It is reported that high content of TS leads to a decrease in the formation of methane due to mass transfer limitations.

The production of VFA from the organic waste has an extensive range of applications which include bioenergy production such as electricity, biohydrogen, and lipids for biodiesel (Lee, 2014). The higher content in acetic or butyric acids in acidification phase is appropriate for methane formation.

8 Models for VFA Production

For the VFA production, the mathematical modeling was used as a method of analysis for degradation kinetics. Various models have been attempted, the development of simulation model involves numerous simplifications concerning the processes that take place in the system. The model includes selected set of variables, defined equations of substrate, and model coefficients. Some of the developed models are described briefly and characterize the operational factors which affected the process (Lokshina, 1996).

8.1 First Order Model

In order to describe the dark fermentation process of primary sludge using the first order reaction is the most common method concerning the initial concentration of potential VFA. In the batch reactor experiment, it has been observed that VFA production start immediately and increases until its maximum concentration achieved which is usually after 8 days. Also, in the hydrolysis process, where lipids and carbohydrates of organics degrade at a faster rate, but protein is the rate-limiting step in the AD which also account for the extensive rate constant of hydrolysis.

8.2 Steady State Acid Fermentation Model

Fermentation of primary sludge from a treatment plant in cape town, South Africa was experimented in a batch reactor to study the effects of solid concentration. The experiment was performed across a range of influent VSS from 11 g VSS/L to 42 g VSS/L. It were noted that fermentation kinetics per unit VSS is independent of VSS concentration with no concentration effect could be detected. The equation 1 below express the VFAs formation is a first order reaction with potential VFAs remaining per initial VSS.

$$\frac{d(VFA'_{tvo})}{dt} = -k * VFA'_{pvo} \quad \text{Eq 1}$$

whereas, VFA'_{tvo} = concentration in mg of VFA as per COD per mg of initial VSS at any time t.

K = first order reaction constant.

VFA'_{pvo} = potential mg of VFA as COD per mg of initial VSS

In order to solve the above expression, VFA'_{pvo} and k should be determined from the experimental result. All the value of VFA'_{tvo} is calculated and plotted against time in the graph. The straight line in the graph yield the best value for VFA'_{pvo} and the k is determined from equation 2 and the slope(m) of the straight line.

$$m = -k * \log_{10} e \quad \text{Eq 2}$$

In the reported value, the maximum potential conversion of influent COD to VFA at 20⁰ C for primary sludge at retention time less than 10 days was 17% (Lilley, 1990). Later, it was recommended that the fermentation system should not exceed 6 days retention time as there may be a methanogenic activity which will reduce the yield of VFA production.

8.3 Anaerobic Digestion Model No 1

The Anaerobic Digestion Model No 1 build based on the Activated Sludge Model. ADM No 1 model uses first order kinetics for the hydrolysis stage and, for a most fundamental approach that can take the range of disintegration processes. Primary sludge and waste activated sludge is assumed to first disintegrate into carbohydrate, protein, and lipid particulate substrate and then undergoes hydrolysis (Albornoz, 2017). The first order disintegration step with respect to the composite waste material is expressed in

$$r_{dis} = k_{dis} * X_{composite} \quad \text{Eq 3}$$

where, r_{dis} = rate of disintegration

k_{dis} = first-order disintegration constant

$X_{composite}$ = composite waste material

After the disintegration of the composite material into carbohydrates, lipids, and proteins three parallel conduits happens to each component. This separation is very important as it will yield the three different products through the hydrolysis of three different conduits.

First order rate of carbohydrate with respect to particulate carbohydrate concentration was expressed in equation 4

$$r_{hyd,ch} = k_{hyd,ch} * X_{ch} \quad \text{Eq 4}$$

where, $r_{hyd, ch}$ = rate of carbohydrate hydrolysis

$k_{hyd,ch}$ = first-order carbohydrate hydrolysis constant

X_{ch} = carbohydrate concentration

The product of equation 4 produces monosaccharides which are uptake by the sugar to produce VFA as described in equation 5.

$$r_{su} = k_{m,su} \frac{S_{su}}{K_s + S_{su}} X_{su} * I_1 \quad \text{Eq 5}$$

Where r_{su} = rate of sugars uptake

$k_{m,su}$ = specific Monod maximum uptake rate constant for sugars

K_s = Monod half-saturation constant

S_{su} = Sugar concentration

X_{su} = sugar degraders

I_1 = Inhibition function

Similarly, first order reaction rate of hydrolysis of proteins and lipids with respect to particulate protein concentration and lipid concentration respectively produce the VFA production when the product of the reaction in equation 6, i.e. amino acids, whose uptake produce VFA from proteins expressed in equation 7

$$r_{hyd,pr} = k_{hyd,pr} * X_{pr} \quad \text{Eq 6}$$

where, $r_{hyd,pr}$ = rate of protein hydrolysis

$k_{hyd,pr}$ = first-order protein hydrolysis constant

X_{pr} = protein concentration

$$r_{aa} = k_{m,aa} \frac{S_{aa}}{K_s + S_{aa}} X_{aa} * I_1 \quad \text{Eq 7}$$

Where, r_{aa} = rate of amino acids uptake

$k_{m,aa}$ = specific Monod maximum uptake rate constant for amino acids

K_s = Monod half-saturation constant

S_{aa} = amino acids concentration

X_{aa} = amino acids degraders

In case of lipids, the product of the reaction produces long chain fatty acids as described in equation 8 whose uptake will produce hydrogen gas and acetate according to the rate as expressed in equation 9.

$$r_{hyd,li} = k_{hyd,li} * X_{li} \quad \text{Eq 8}$$

where, $r_{hyd,li}$ = rate of lipids hydrolysis

$k_{hyd,li}$ = first-order lipids hydrolysis constant

X_{li} = lipids concentration

$$r_{fa} = k_{m,fa} \frac{S_{fa}}{K_s + S_{fa}} X_{fa} * I_1 \quad \text{Eq 9}$$

where r_{fa} = rate of fatty acids uptake

$k_{m,fa}$ = specific Monod maximum uptake rate constant for fatty acids

K_s = Monod half-saturation constant

S_{fa} = fatty acids concentration

X_{fa} = Long-chain fatty acid degraders

The main disadvantage of this method is that the substrate fraction of carbohydrate, protein and lipid content must be characterized which is very difficult in routine practice. Another drawback for the first-order model is that there is no limit for maximum rate whereas, the equation suggests an increase in component would increase the rate infinitely (Albornoz, 2017).

8.4 Surface Limiting Model

Surface limiting model is an alternate model to measure the rate of hydrolysis as a function of the biodegradable particulate substrate for surface limiting model. This observation was regarded as surface limiting model, causing mass transfer limitations. The aim of this model was to actually reduce the number of variables while still producing VFA. In this model, instead of distinguishing individual VFA, the sum of VFA was considered. The equation 10 below shows that mass balance equation for VFAs in the model

$$\frac{dC_{VFA}}{dt} = \frac{1}{HRT} (C_{VFA}^{in} - C_{VFA}) + (1 - Y_a) * r_{x,a} - r_{x,m} \quad \text{Eq 10}$$

where C_{VFA} = concentration of VFA

Y_a = acidogenic biomass yield

$r_{x,a}$ = reaction rate for acidogenic biomass growth

$$r_{x,a} = U_{max,a} \frac{C_{mo} \quad C_{NH4-N}}{(K_a + C_{mo})(K_n + C_{NH4-N})} C_{x,a} \quad \text{Eq 11}$$

$r_{x,m}$ = reaction rate for methanogenic biomass growth

$$r_{x,m} = U_{max,m} \frac{C_{mo} \quad C_{NH4-N}}{(K_a + C_{mo})(K_n + C_{NH4-N})} C_{x,m} \quad \text{Eq 12}$$

It was found that surface limiting model was able to explain and describe the steady state result with respect to the effect of retention time over 3.5 days on effluent VFA (Albornoz, 2017) but model did not consider the effects of mixing intensity, temperature and chemical inhibitors on the rate of VFA production (Münch, 1999)

9 Material and Methods

This section describes the apparatus and methods that were employed to analyze the semi-continuous fermentation process using source separated organics as substrate. This experiment was performed for the production of volatile fatty acids for raw and pre-treated source separated organics. The pre-treated SSO sample was hydro-thermalized at 170 °C as described in section 9.3. (Lokshina, 1996)

Table 1: Average properties of feed source separated organics

Average properties of feed source separated organic		
Parameters	Raw SSO	Pre-treated SSO
pH	5.55	5.45
TSS (mg/L)	62242	42904
VSS (mg/L)	45383	30967
SCOD (mg/L)	32498	47950
TCOD (mg/L)	99183	98617
Ammonia (mg/L NH ₃ -N)	867	927

9.1 Substrate

In this experiment, Source Separated Organic (SSO) was used as the feedstock for the fermentation process. Source Separated Organics was obtained from Disco Road facility and stored separately in a refrigerator that keeps the samples at 4⁰ C. Disco road facility rolled out in 2002 and Source Separated Organic mostly consists of food waste, pet waste, wet paper, sanitary products and household plants, etc.

9.2 Experimental set-up and procedures

The experimental work was initiated by feeding the digesters with SSO (raw and pre-treated) to study the fermentation process under anaerobic condition. Figure 6 displays the experimental set-up of SSO raw and SSO pre-treated reactor with a working volume of 1.5 litres each. The temperature was maintained at 38⁰ C (mesophilic) using a water bath tub. The reactors were equipped with stir to maintain homogeneity at 150 rpm. Also, the tedler gas bag was connected to the reactor to check for methane production.

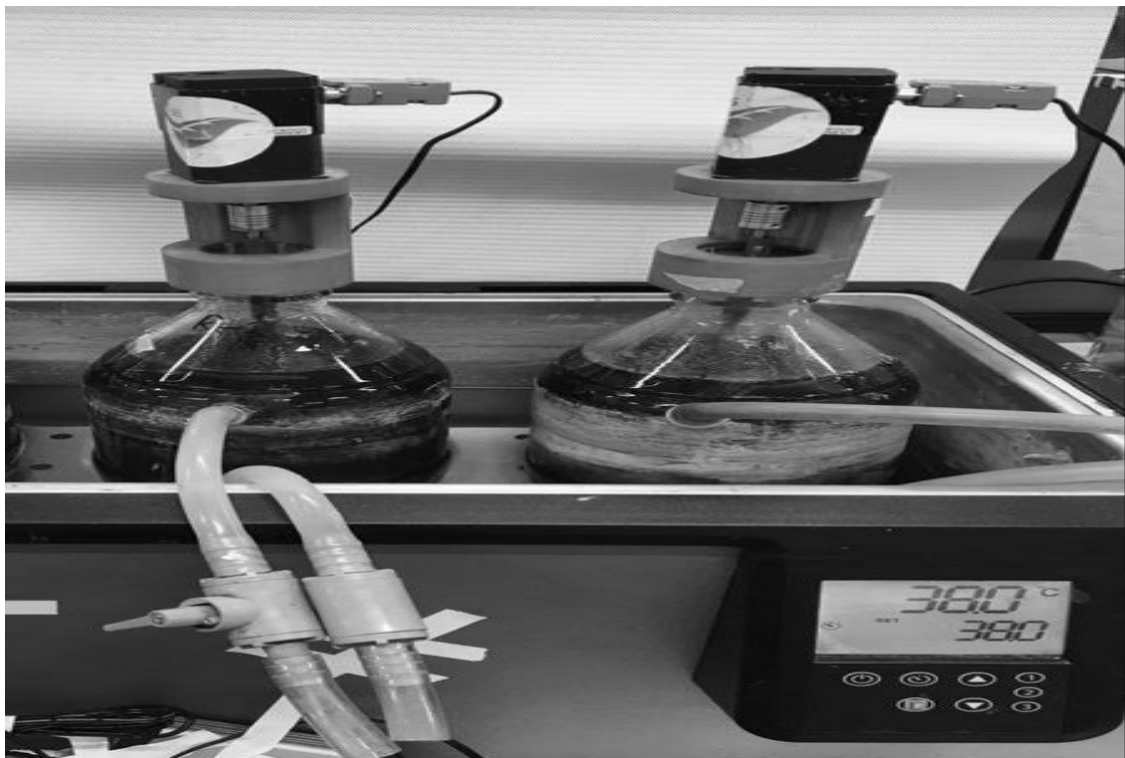


Figure 6: Experimental anaerobic digester setup. Raw (left) & pretreated (right) SSO.

During feeding, the reactors headspace was purged with nitrogen gas in order to maintain anaerobic condition and to prevent vacuum formation in the digester. Each digester had two valves, lower one for sampling and upper one for feeding. Sampling and feeding were performed using the syringe pump. Every day 500 ml out of 1500ml substrate was taken out, and a new 500 ml substrate was fed into the digester in order to maintain retention time for 3 days and, the experiment was run for 6 weeks.

Table 2: Frequency of sample analysis

The frequency of sample Analysis		
Activities	Influent	Effluent
Feeding	Everyday	Everyday
Chemical Oxygen Demand	Once a week	Twice a week
VFA	Once a week	Twice a week
Ammonia	Once a week	Twice a week
Alkalinity	Once a week	Twice a week
Carbohydrates	Once a week	Twice a week

9.3 Hydro-thermal procedure

Hydrothermal pre-treatment was done by Parr 4848 Hydrothermal Reactor with a capacity of 2 L at one time of operation. However, the volume of each pre-treatment in this study was 1.5 liter. The heating rate of materials initially were 2 °C per minute and then was reduced to 1 °C per minute. During the pre-treatment, the SSO was constantly mixed and operated by specView Parr 4848 controller and hydrothermal pre-treatment rate was recorded accordingly.

In the hydro-thermal process, the raw sludge was treated at 170⁰ C. Figure 7 Shows the hydro-thermal set-up. It was run on ramp/soak pattern. The pattern consisted of 4 steps raising the temperature from 20⁰ C to 170⁰ C in certain time periods as shown in figure 8. To bring the substrate to room temperature, another setup for cooling the system was attached to the hydro-thermal and, also can be seen in figure 9 that after reaching 170⁰ C temperature graph significantly fall to room temperature.



Figure 7 : Parr 4848 pressure reactor

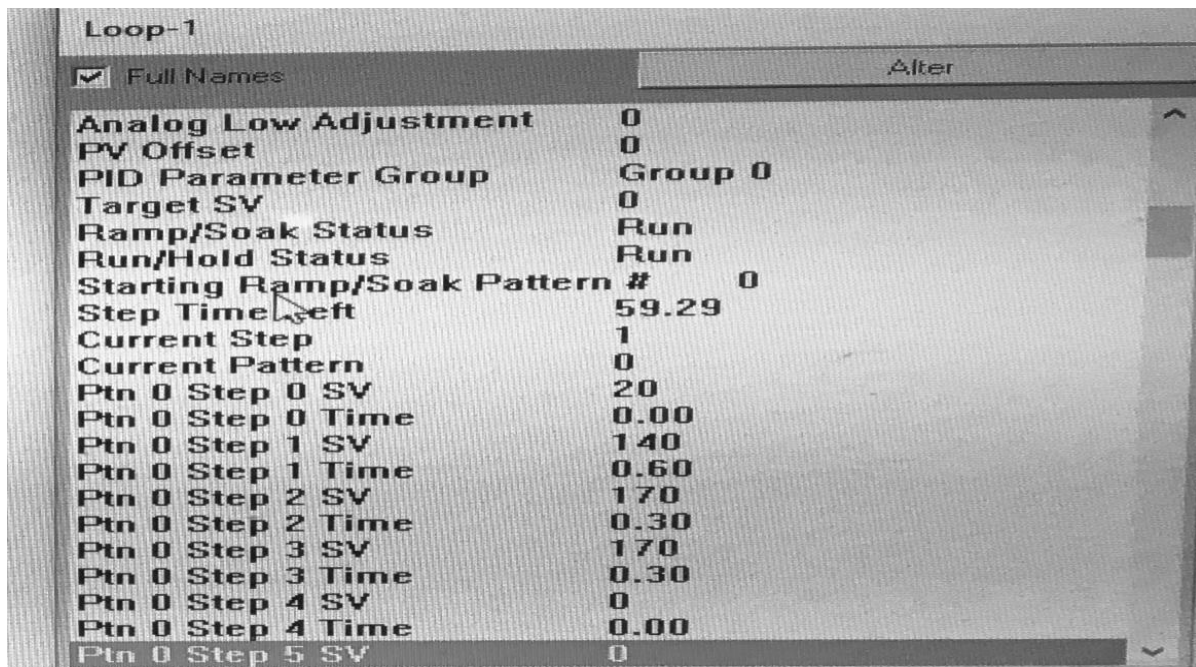


Figure 8: Temperature pattern for hydro-thermal

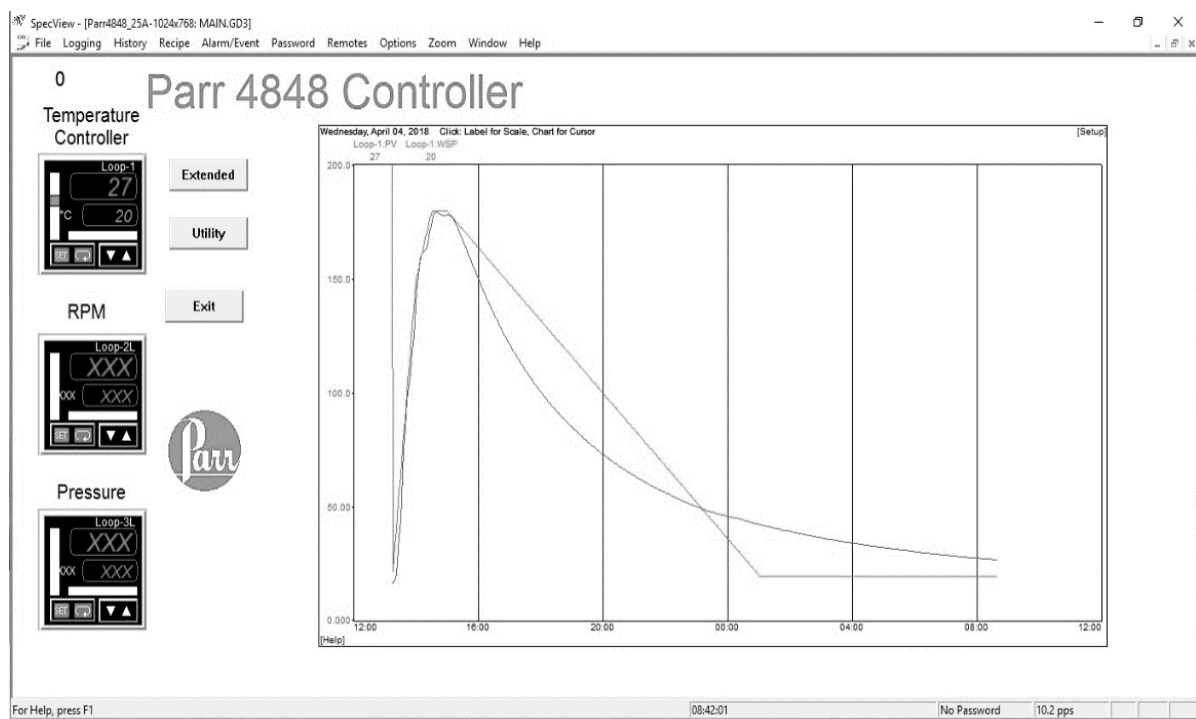


Figure 9: Parr 4848 controller showing temperature graph

10 Sample Analyses

All the analyses that were completed and carried out in triplicates, the complete procedure for each test are listed below.

10.1 pH

The pH of each sample was measured immediately; it was collected using VWR Benchtop pH Meter and refillable glass probe, model AB15 as shown in figure 10 was employed to measure pH for all the samples. This meter was calibrated twice a week with pH reference standards.

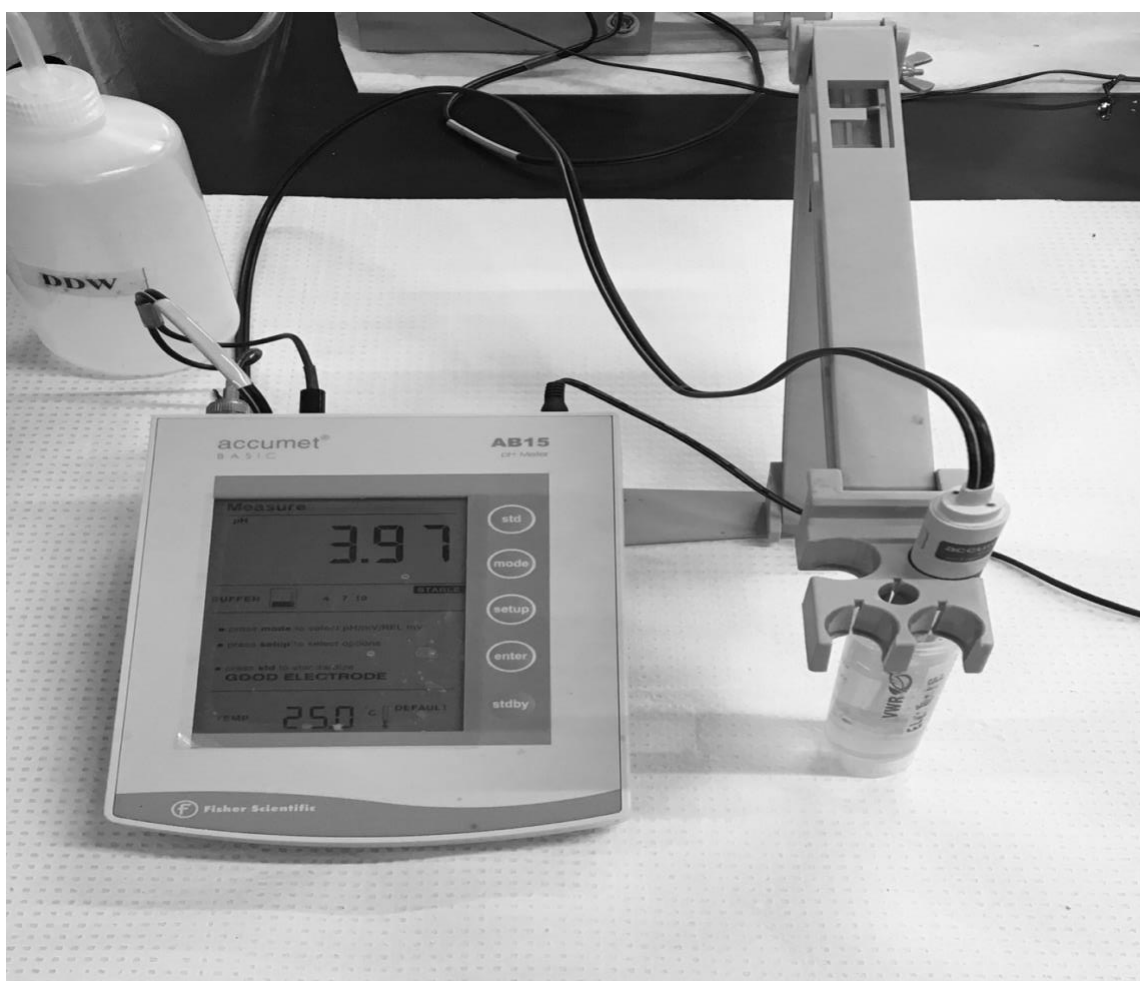


Figure 10: pH meter fisher scientific model AB 15

10.2 TS/VS

The standard guidelines were followed provided in 2540B and 2540E for TS and VS respectively.

10.3 TSS/VSS

Standard methods 2540D and 2540E was employed to measure TSS and VSS respectively. 2 ml of each sample using 1.5 μm glass microfiber filter paper for filtration and then drying in the oven at 105⁰ C for 1 hour for TSS. The mass of the samples was measured and was placed in a furnace for 20 minutes at 550⁰ C. After combustion, plates were measured, and the weight loss represented as VSS.

10.4 Chemical Oxygen Demand (Total / Soluble)

High range (20- 1500mg/L) COD reagent vials from HACH were used to follow method 8000. For sample analysis, the tests were conducted in triplicates. For soluble COD, the sample was centrifuged at 9800 rpm for 30 minutes as shown in figure 11. After centrifuged, the sample was filtered with 0.45 μm and diluted with an appropriate dilution factor. 2 ml of diluted sample was added to the vial and blank was also prepared for 2 ml of DDW. The vials were inverted 10 times before digestion in the COD reactor for 2 hours at 150⁰ C. The samples were measured using HACH DR 3900 spectrophotometer.

10.5 Ammonia

High range (0.4 – 50 mg/L) Amver Ammonia reagent set were used as per Method 10031, the Salicylate method. Concentrations of ammonia were determined using the HACH DR3900 spectrophotometer.

10.6 VFA

Esterification method TNT 872 reagent set (range 50 to 2500 mg/L) were used as per standard method 10240. Concentrations of volatile acids were determined using the HACH DR3900 spectrophotometer.



Figure 11: Thermo fisher scientific centrifuge machine

10.7 Carbohydrates (Total / Soluble)

The carbohydrates concentration is measured calorimetrically as glucose because SSO mainly constitute of food waste, using the phenol-sulfuric method. A standard calibration curve with glucose at concentrations of 5-1000 mg /L must be prepared. Deionized water is used as blanked. The reagent used was standard glucose, concentrated sulfuric acid, phenol 5 % w/v (weight/volume).

10.8 Alkalinity

High range (25 - 400 mg/L CaCO_3) total Alkalinity TNT 870 reagent set were used as per method 10239. Moreover, the concentration of Alkalinity was determined using Hach DR3900 spectrophotometer.

11 Results and discussion

Figure 12 shows the average result of TS and VS which was done in triplicate for the raw and pre-treated samples.

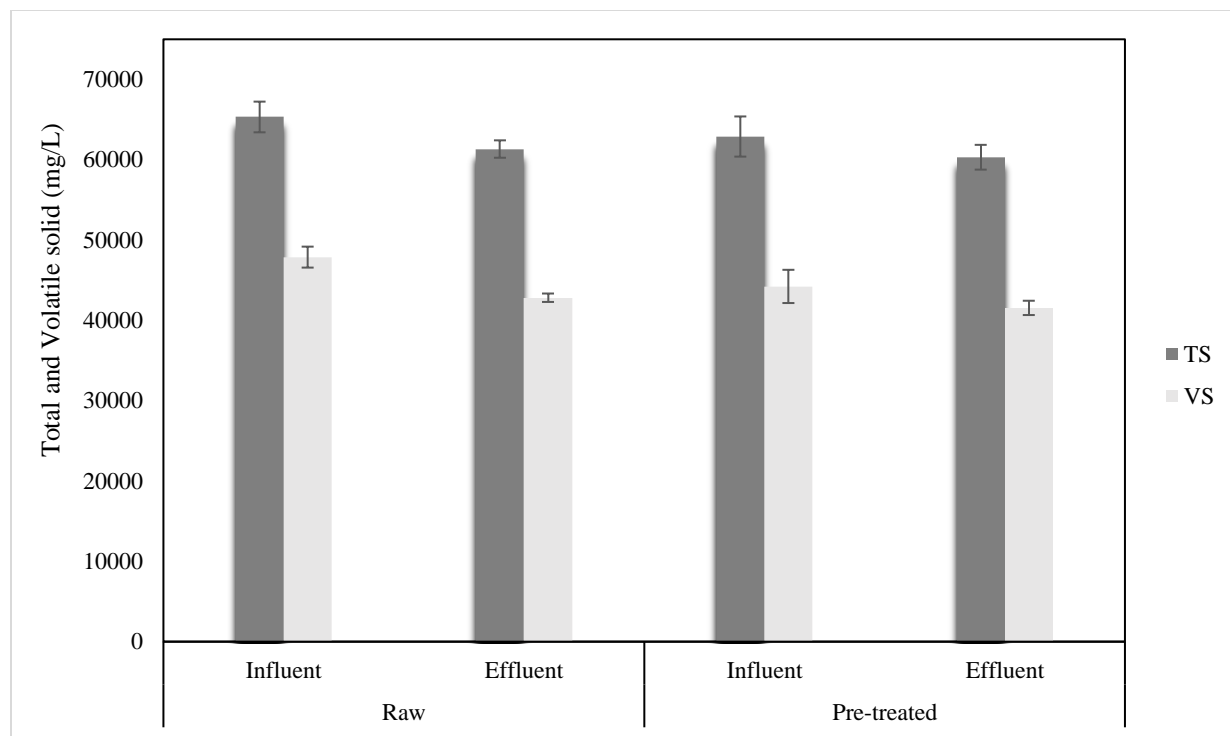


Figure 12 : Total & volatile solid of raw & pre-treated SSO

The TS value of raw and pre-treated sample shows almost the same value. The highest range of 65330 mg/L of TS is from the raw influent. The slight decrease in both raw effluent and pre-treated effluent sample value is due to the continuous mixing in the digester. The pre-treated sample is more soluble, so the value of TS for raw and pre-treated samples observed decrease from 62896 mg/L to 60316 mg/L respectively.

For VS, it shows the same behaviour as of TS, but the highest value for VS is 47880 mg/L from the raw influent. Effluent in both the cases, i.e. raw and pre-treated observed slight decrease from its influent value. For raw sample, 47880 mg/L to 42823 mg/L and, pre-treated 44231 mg/L to 41559 mg/L.

The average result of TSS and VSS which was done in triplicate of raw and pre-treated samples are dramatize in figure 13.

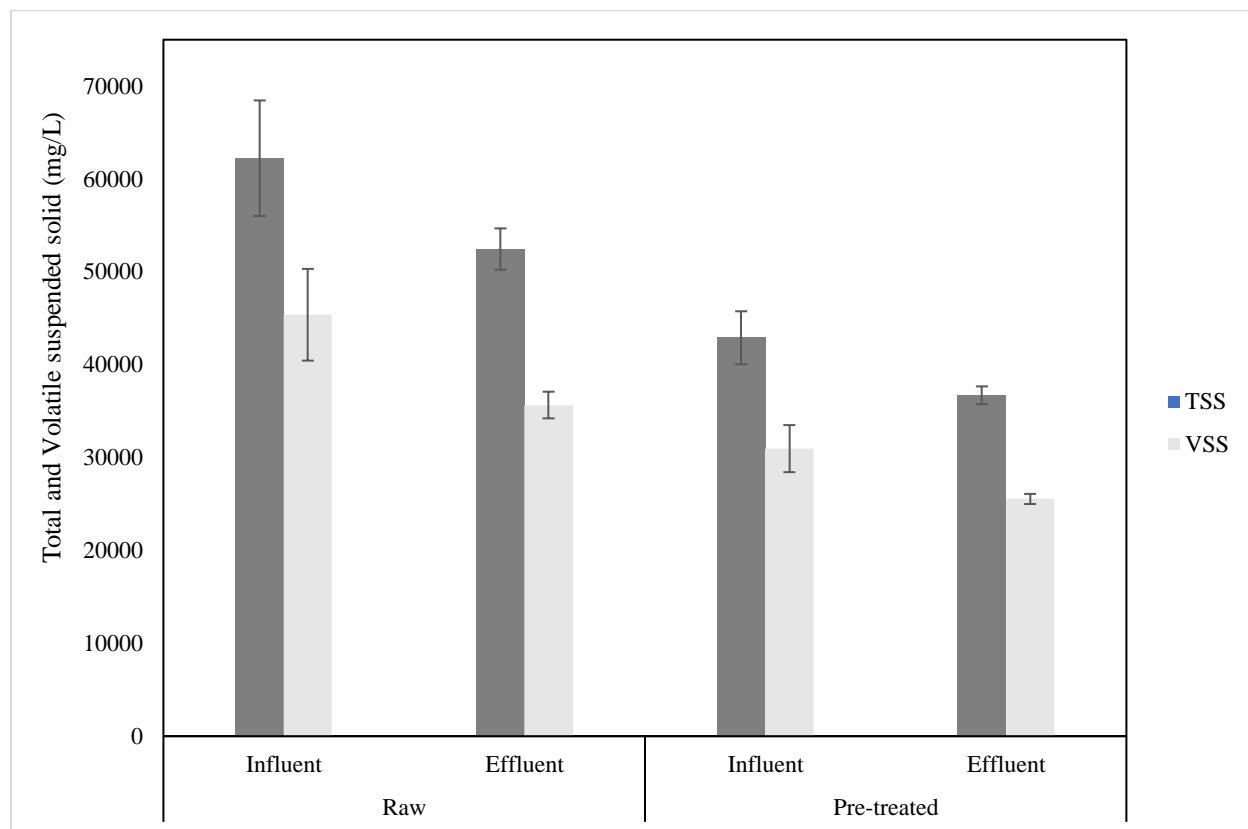


Figure 13: Total & volatile suspended solid of raw & pre-treated SSO

The figure 13 shows that the average value for TSS in raw influent is very high with a value of 62242 mg/L as comparative to all. Raw effluent observes a decrease in value to 52454 mg/L as the substrate was continuous mixing in the reactor with retention time for 3 days which make it more soluble. In the pretreated sample, the substrate was treated at a high temperature of 170⁰ C, so the value of TSS of the pretreated sample, influent with a value of 42904mg/L reduces to the value of 36712 mg/L for effluent.

The average volatile suspended solids show the same behaviour as that of average total suspended solids. The value of raw influent 45383 mg/L decreased to a value of 35665 mg/L in the raw effluent. In the pre-treated sample, the value of influent 30967 mg/L decrease to 25547 mg/L in the effluent.

The average result of Total Chemical Oxygen Demand (TCOD) are presented in figure 14 for raw and pre-treated samples which was done in triplicate.

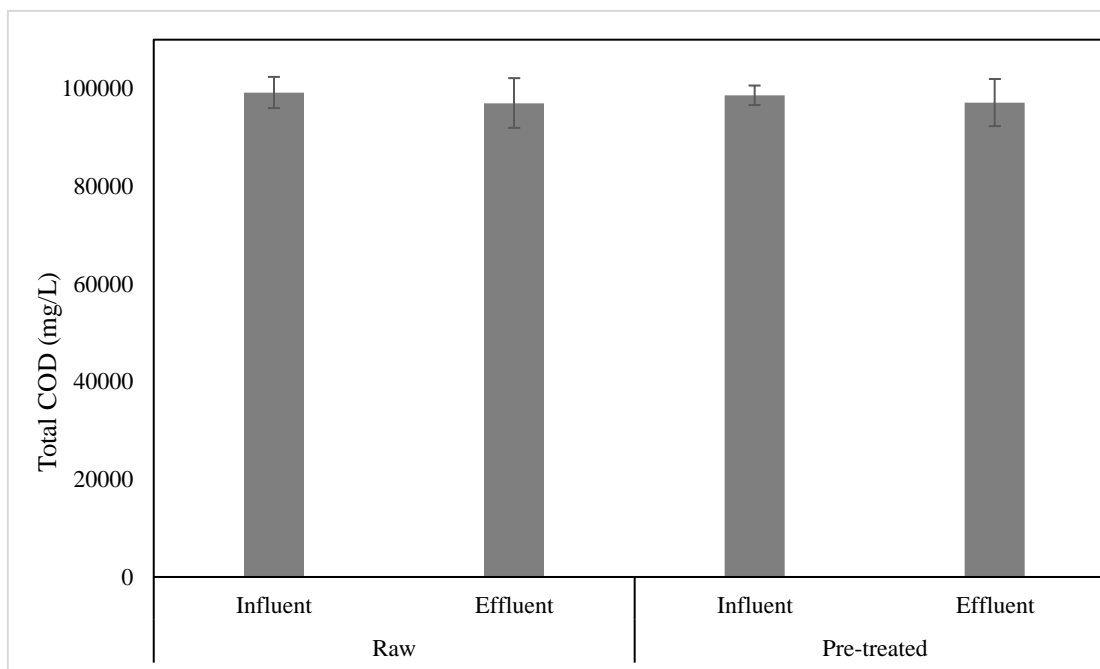


Figure 14: Total chemical oxygen demand of raw & pre-treated SSO

The figure 14 shows that there is no big difference in the concentrations of the raw and pre-treated sample for both influent and effluent. For a raw sample, influent analysis with the value of 99183 mg/L reduced to effluent with a value of 97033 mg/L. This little change also indicates that the fermentation process was preventing methanogenesis were methane production takes place.

For a pre-treated sample, the value of influent 98617mg/L gives the effluent with a value of 97125 mg/L. Total COD should be conserved in fermenters because the hydrolysis process only converts particulate COD into Soluble COD.

Figure 15 shows the average result for Soluble Chemical Oxygen Demand (SCOD) which was done in triplicate for raw and pre-treated samples.

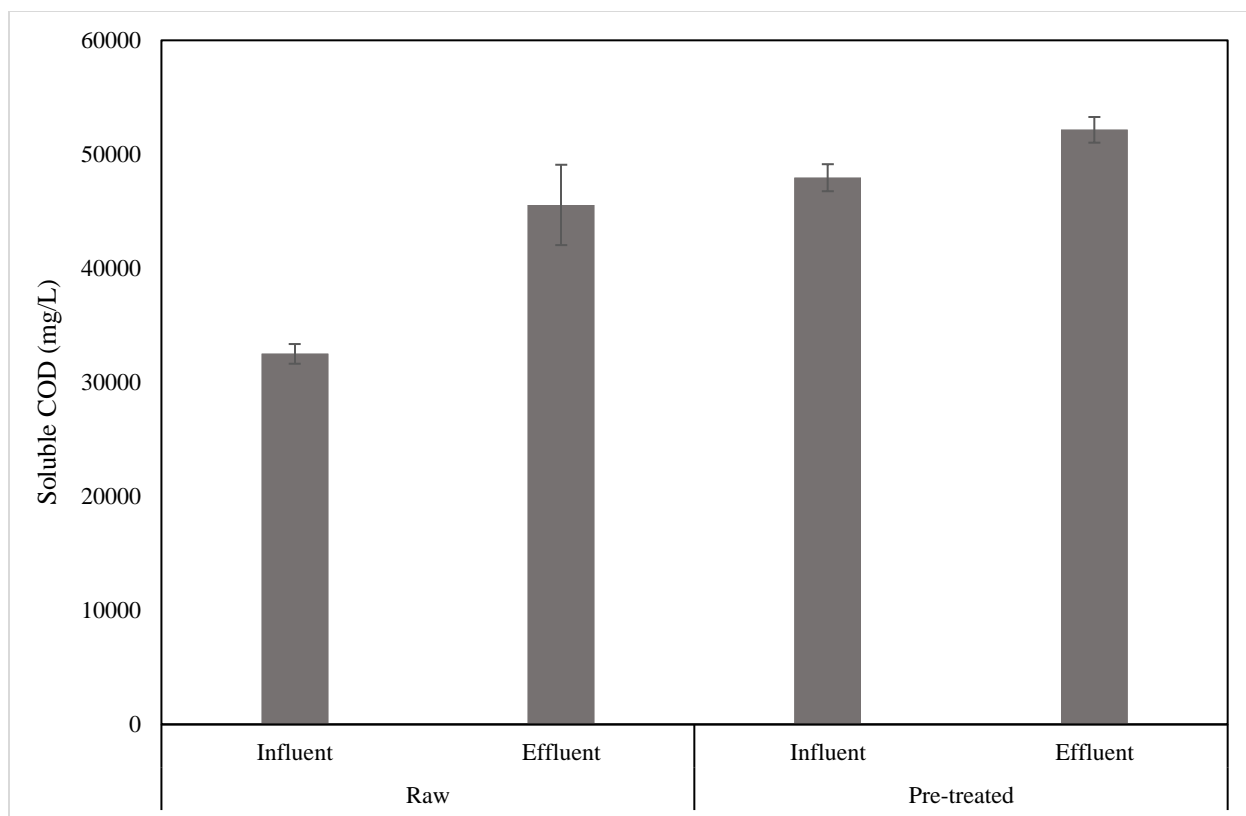


Figure 15: Soluble chemical oxygen demand of raw & pretreated SSO

Figure 15 shows a significant increase in the raw sample for influent to effluent value. There is an increase from raw influent to pre-treated influent because the hydro-thermal process makes the substrate more soluble which increases its value. The value of raw influent 32498 mg/L rises to 45563 mg/L for raw effluent. This change is due to a small amount of methanogenic activity.

For a pre-treated sample, there was a slight increase in average value from influent to effluent; the value changes from 47950 mg/L to 52150 mg/L respectively. This is a good indication that there was minimal COD loss to methanogenesis.

Figure 16 shows the average result for Total Carbohydrates which was done in triplicate for raw and pre-treated samples.

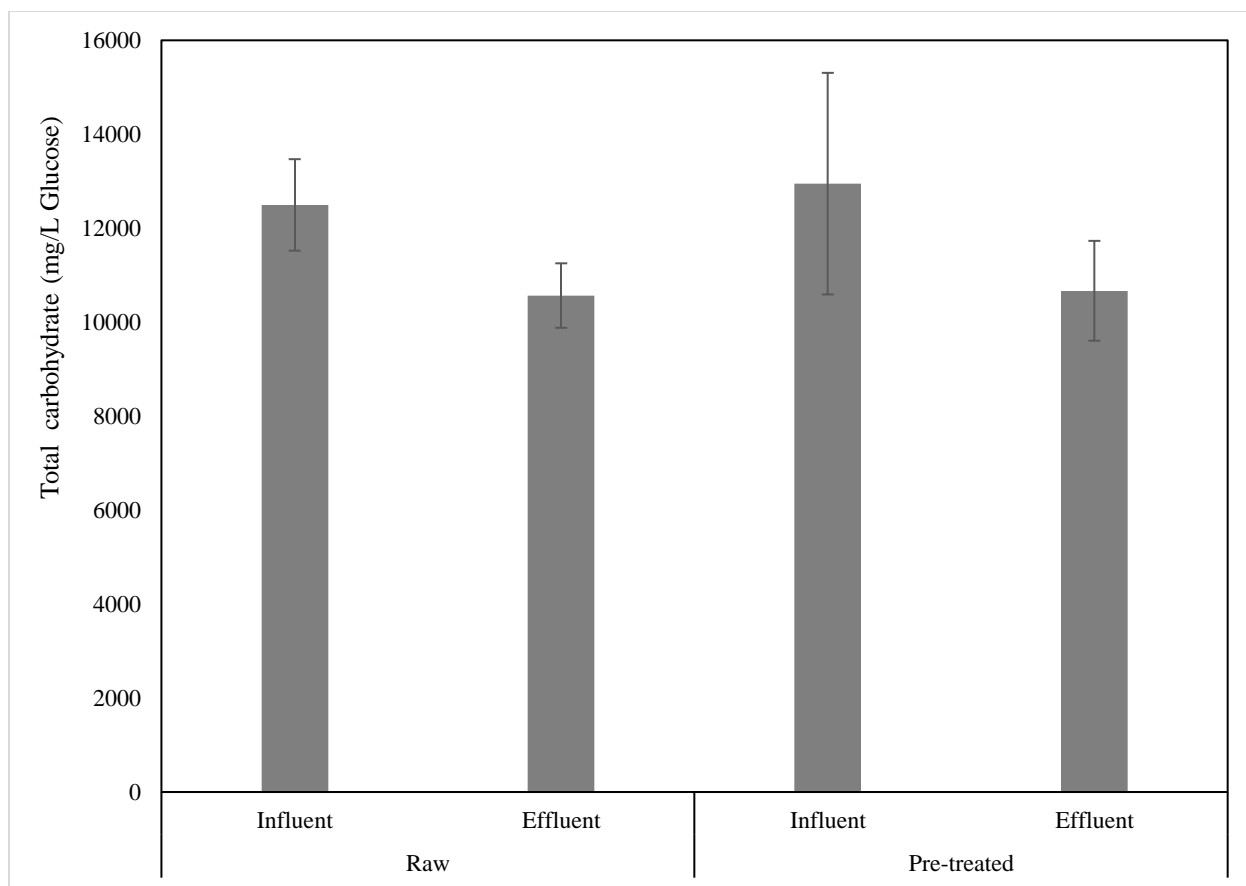


Figure 16: Total carbohydrates of raw & pre-treated SSO

Figure 16 shows the average result for total carbohydrates for the raw and pre-treated sample. The concentration of total carbohydrates reduces in effluent which shows that there is the production of VFA.

In the raw sample, the value of influent 12496 mg/L reduces to 10567 in the effluent.

In the pre-treated sample, the influent value of 12949 mg/L falls to the value of 10668 mg/L in the effluent.

Figure 17 shows the average result for Soluble Carbohydrates which was done in triplicate for raw and pre-treated samples.

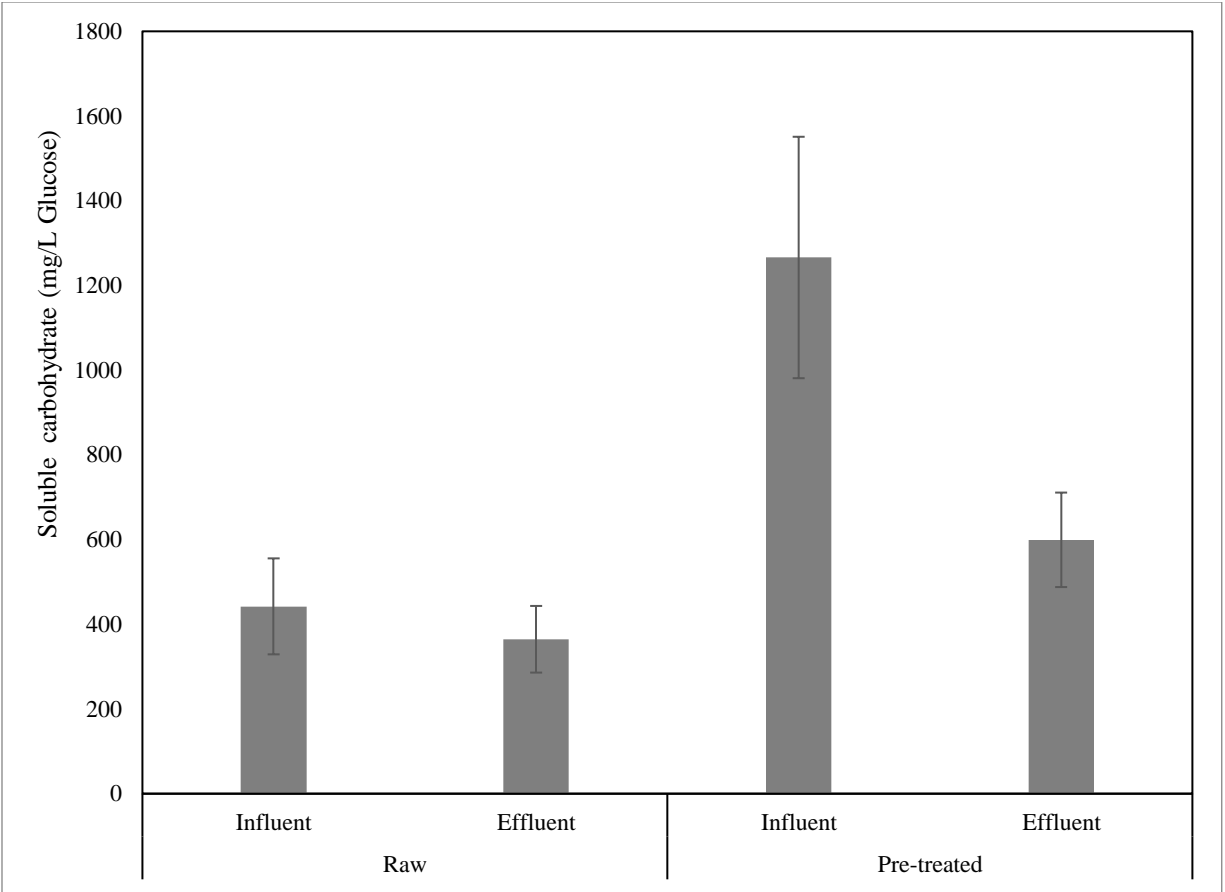


Figure 17: Soluble carbohydrates of raw & pre-treated SSO

The figure clearly shows that in the pre-treated sample, there is a drastic decrease from influent to effluent because the hydro-thermal makes the substrate more soluble and carbohydrates are converted into VFA in large amount in the fermentation process. In the raw sample, there is not much change in average concentration from influent to effluent. In the pre-treated sample, the influent value of 1266 mg/L significantly reduces to 599 mg/L because of VFA production.

Figure 18 shows the average result for alkalinity which was done in triplicate for raw and pre-treated samples.

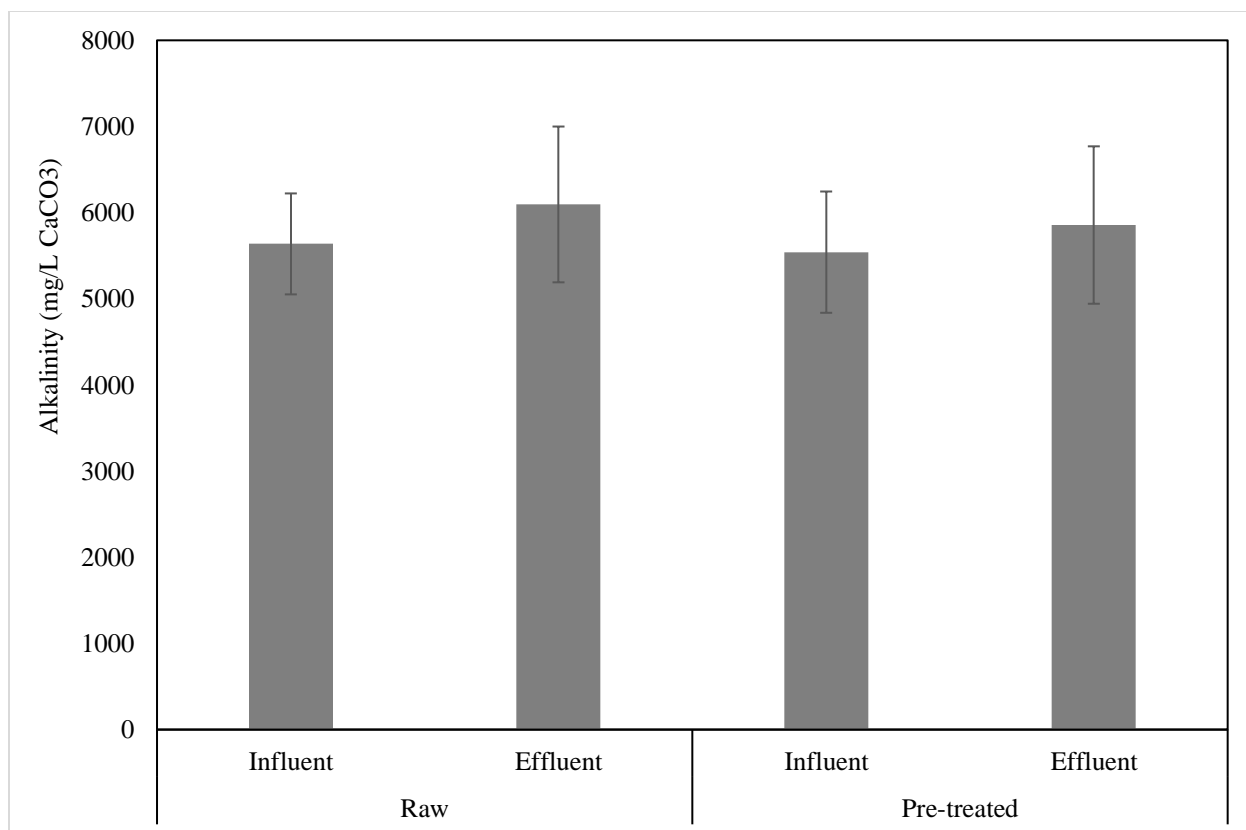


Figure 18: Alkalinity of raw & pre-treated SSO

Alkalinity was very often used as a pointer of biological activity. Increase in Alkalinity means more biological processes. Figure 18 shows a slight increase in alkalinity concentration after fermentation proces. In the raw sample, a slight rise in influent to effleunt was observed with the value from 5637 mg/L to 6095 mg/L. In the pre-treated sample, like raw sample, there was a slight increase in the value from influent to effleunt.

Figure 19 shows the average result of ammonia which was done in triplicate for raw and pre-treated samples

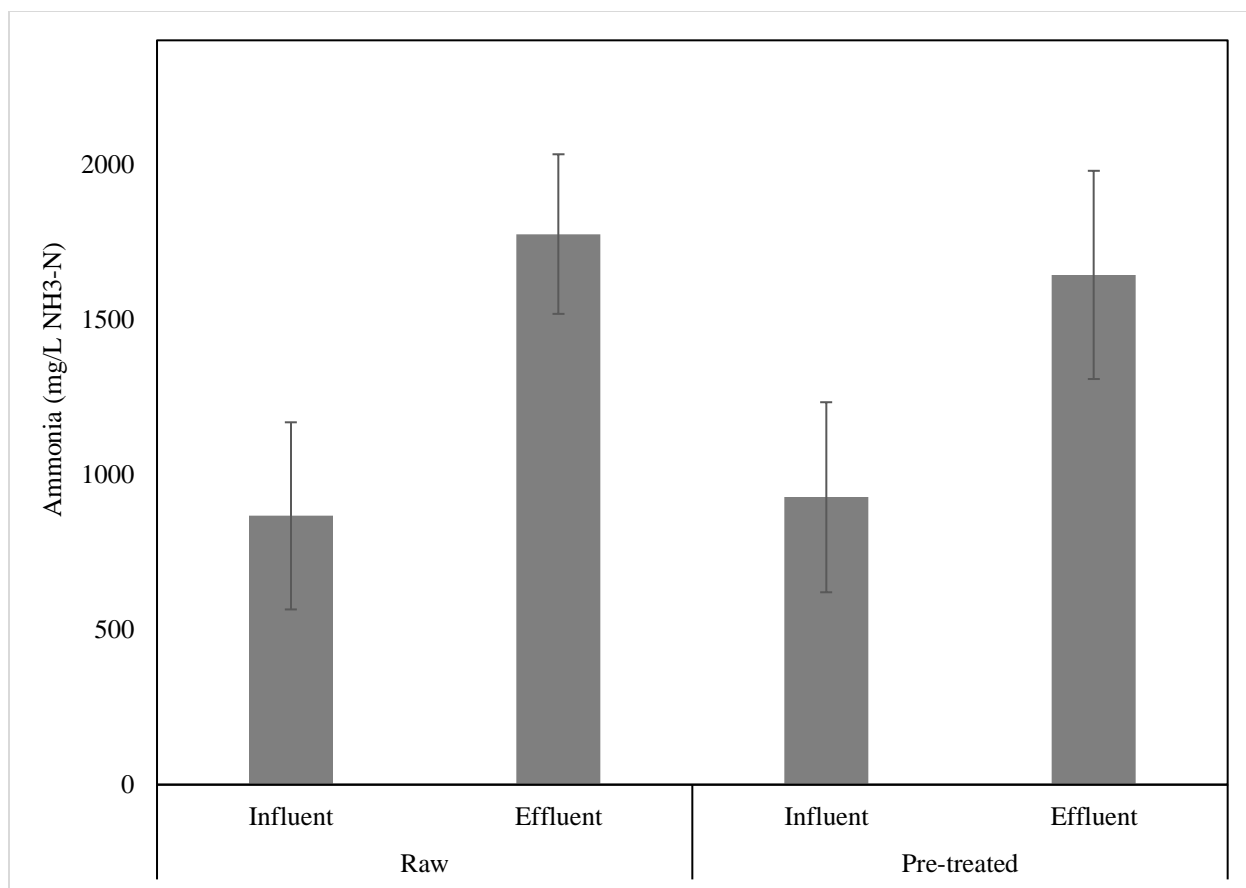


Figure 19: Ammonia of raw & pre-treated SSO

Figure 19 demonstrate that average value for ammonia increased in the effluent for both raw and pre-treated sample. For a raw sample, an increase of influent from 867 mg/L to effluent 1775 mg/L was noted. For a pre-treated sample, the increase of influent from 927mg/L to effluent 1644 mg/L was observed. The increase in the value of the ammonia also indicates that in the fermentation process, ammonia production is high.

Figure 20 shows the average result for Volatile Fatty Acids (VFA) which was done in triplicate for raw and pre-treated samples.

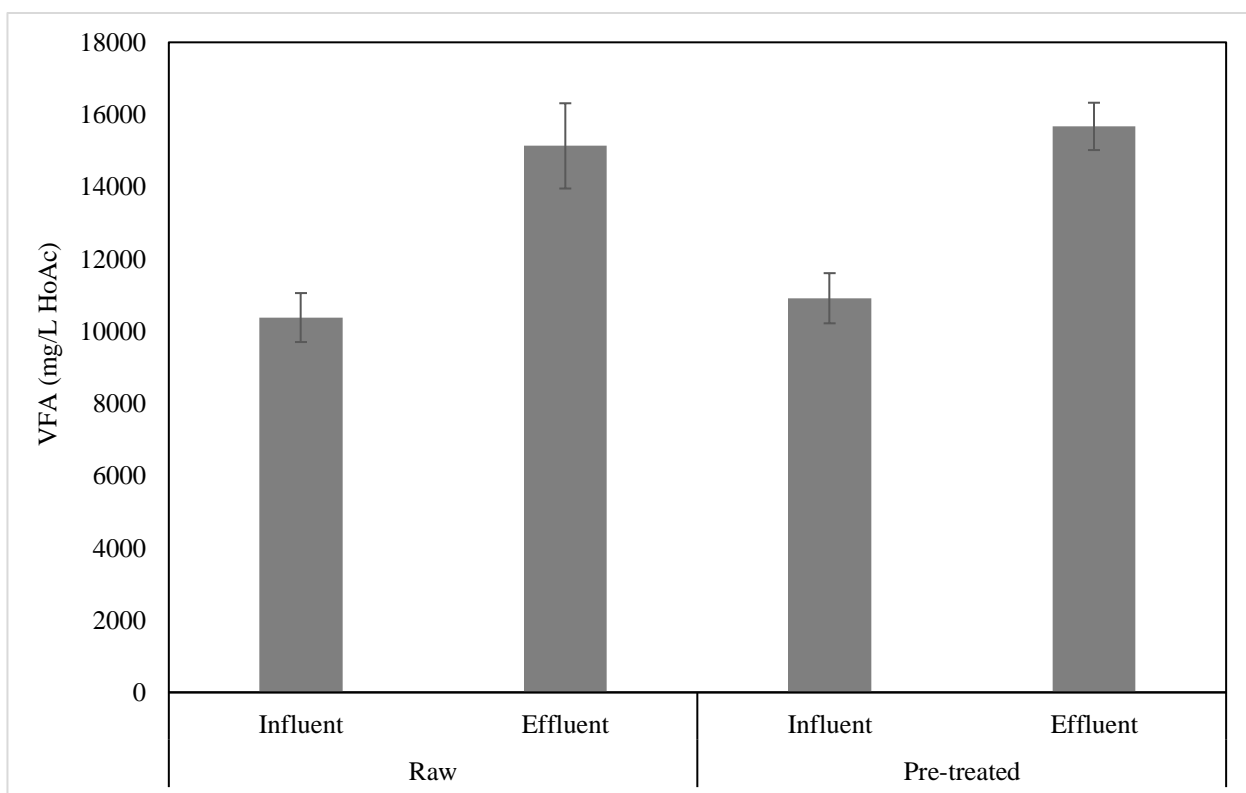


Figure 20: VFA of raw and Pre-treated SSO

Figure 20 shows the result of average volatile fatty acids in raw and hydro-thermalized or pre-treated sample. In the fermentation process, VFAs are produced and increase in the value of effluent marks this statement. Volatile fatty acids are the rich amount in SSO, but the fermentation process helps. High production of VFA was noted in pre-treated effluent with a value of 15672 mg/L.

On an average, both raw and pre-treated sample produces almost the same VFA in the fermentation process. In the raw sample, the influent of 10379 mg/L rise to 15133 mg/L in effluent whereas in the pre-treated sample, the influent with 10914 mg/L increases to 15672 mg/L.

Figure 21 shows the result for degree of solubilization in percentage for different processes.

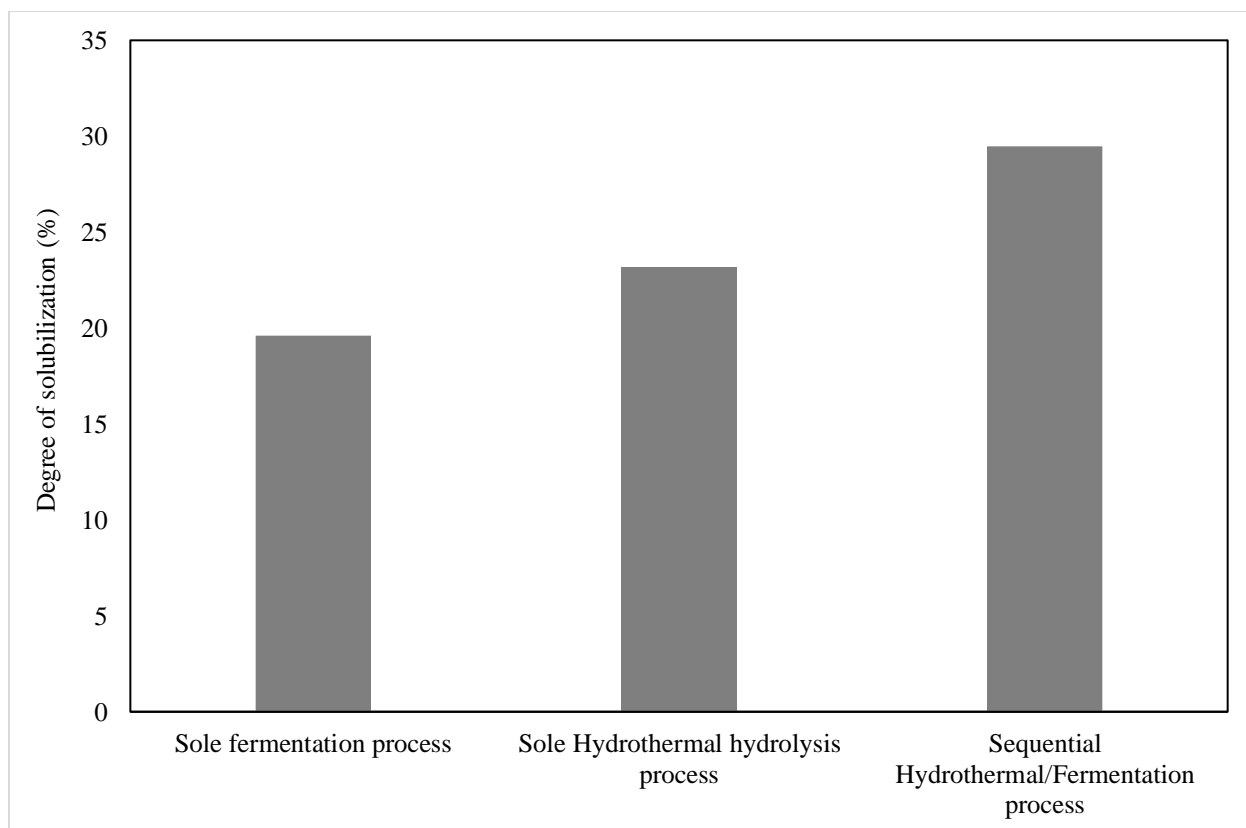


Figure 21: Degree of solubilization of SSO versus Percentage

The result indicate that COD mass balance conditions for hydrolysis and fermentation were favorable. The degree of solubilization of organic material yield more by sequential hydrothermal and fermentation process. The yield was calculated using the ratio of soluble COD and total COD as shown below.

$$\text{SCOD}(\text{yield}) = \frac{\text{SCOD}(\text{effluent})}{\text{TCOD}(\text{influent})}$$

Figure shows that degree of solubilization for sole fermentation is 20%, where as in combined hydrothermal and fermentation process the degree of solubilization increased by 9% from fermentation process. On comparing, fermentation process versus hydrothermal process increases only 3% in hydrothermal process.

Figure 22 shows the result for suspended solids reduction in percentage for different processes.

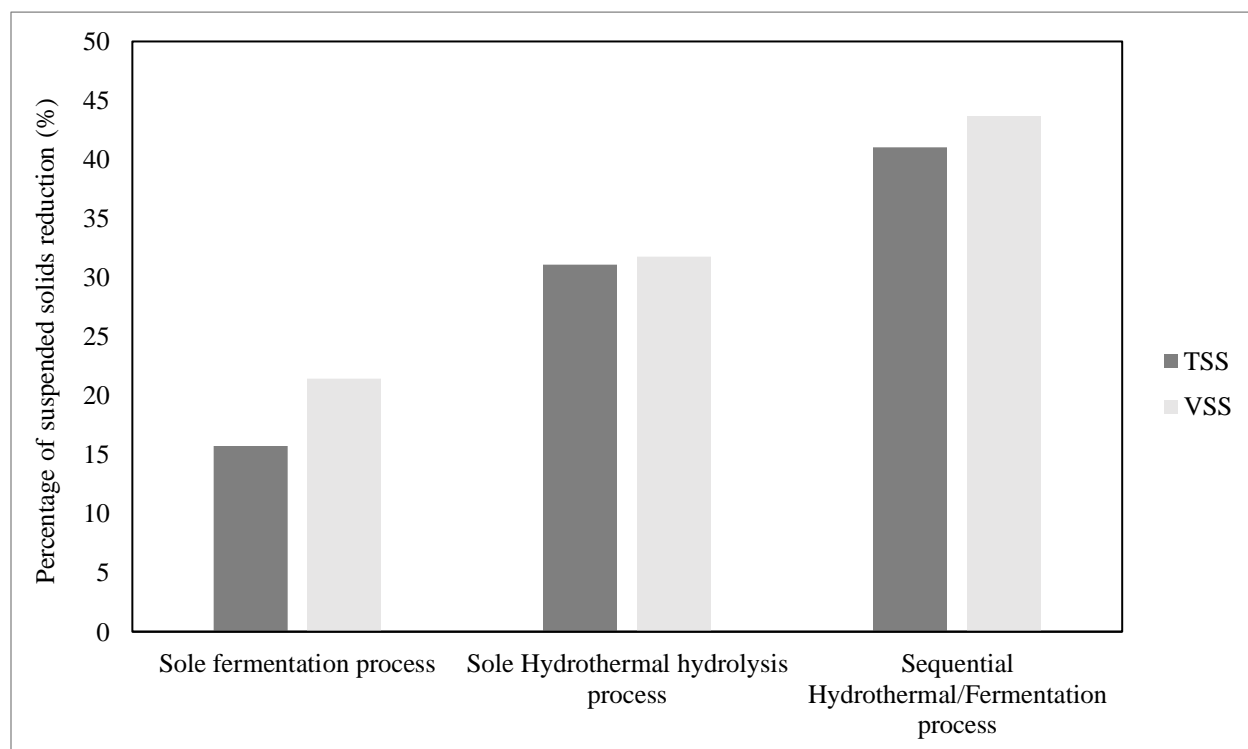


Figure 22: Fermentation process versus percentage of suspended solid reduction

In this figure, reduction of suspended solids in TSS/VSS for three different processes namely sole fermentation process, sole hydrothermal process and combined hydrothermal and fermentation process is shown. It can be clearly depicted from the figure that combination of hydrothermal and fermentation process shows high reduction of suspended solids with 44% for TSS and 41% for VSS because of increase in solubilization. The reduction of suspended solids in fermentation process for TSS and VSS are 16% and 21% respectively. In hydrothermal process, reduction of suspended solids increased as the substrate is more soluble after the hydrothermal treatment and, hence it shows suspended solids reduction by 31% for TSS and 32% for VSS. Also, the tedler bag connected to reactor did not observe evident production for methane gas.

12 CONCLUSION

In this study, the production of volatile fatty acids from source separated organics for pre-treated and raw sample is analyzed using semi-continuous reactor.

First, the results show that hydrothermal process increases the productivity of the VFAs. The VFA produced in the pre-treated sample were high from those of raw sample. Increase in almost 50% of VFA was noted from raw influent to pre-treated effluent. Second, the result for degree of solubilization was increased during hydrothermal and fermentation process, which also help to improve the production of VFA. Also, reduction of suspended solids was noticed to be increased significantly in hydrothermal and fermentation process.

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Glossary

AD	-	Anaerobic Digestion
ADM1	-	Anaerobic Digestion Model No 1
BOD	-	Biochemical Oxygen Demand
CHP	-	Combined Heat and Power
COD	-	Chemical Oxygen Demand
HRT	-	Hydraulic Retention Time
MSW	-	Municipal Solid Waste
OLR	-	Organic Loading rate
pH	-	power of Hydrogen
PHA	-	Poly-Hydroxy-Alkanoates
SCOD	-	Soluble Chemical Oxygen Demand
SRT	-	Solid Retention Time
SSO	-	Source Separated Organics
TCOD	-	Total Chemical Oxygen Demand
TS	-	Total solid
TSS	-	Total Suspended Solid
VFA	-	Volatile Fatty Acid
VSS	-	Volatile Suspended Solid